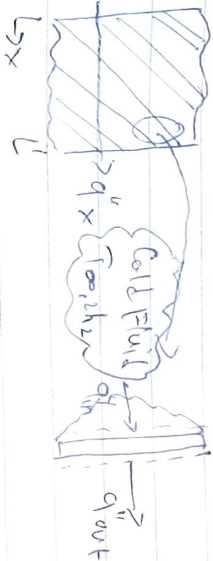


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1) Dik: Satu dimensi, sisi dinding memisahkan aliran panas dan dingin $T_{\infty,1}$ dan $T_{\infty,2}$ masing-masing
Dit: Distribusi temperatur, $T(x)$ dan heat flux, q_x dengan ketebalan $T_{\infty,1}, T_{\infty,2}, h_1, h_2, k$ dan L

Jawab



asumsi 1. Kondisi Satu dimensi

2. Kondisi Steady

3. Constant

4. Radiasi diabaikan

5. Tidak ada generation

$$T(x) = C_1 x + C_2$$

$$-k \frac{dT}{dx} \Big|_{x=0} = h_1 [T_{\infty,1} - T(0)] \quad -k \frac{dT}{dx} \Big|_{x=L} = h_2 [T(L) - T_{\infty,2}]$$

Por BC at $x: L$ to find

$$-k C_1(1) = h_2 [C_1(1) - T_{\infty,2}]$$

$$C_1 = - \frac{(T_{\infty,1} - T_{\infty,2})}{\left[\frac{1}{h_1} + \frac{1}{h_2} + \frac{L}{k} \right]}$$

$$C_2 = - \frac{(T_{\infty,1} - T_{\infty,2})}{\left[\frac{1}{h_1} + \frac{1}{h_2} + \frac{L}{k} \right]} + T_{\infty,1}$$

$$T(x) = \frac{(T_{\infty,1} - T_{\infty,2})}{\left[\frac{1}{h_1} + \frac{1}{h_2} + \frac{L}{k} \right]} \left[\frac{x}{L} + \frac{1}{h_1} \right] + T_{\infty,1}$$

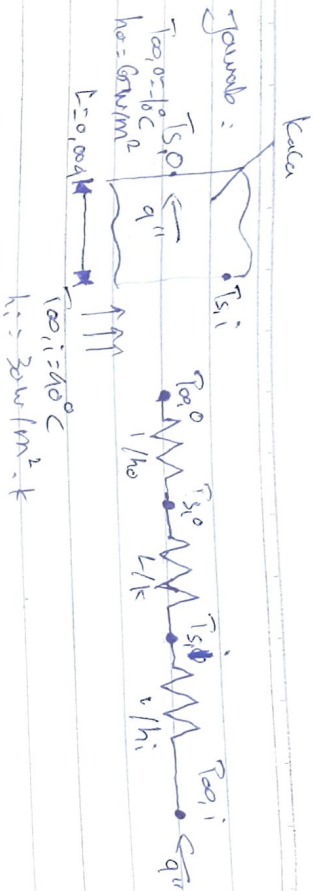
menurut hukum Fourier, heat flux constant dan jadi:

$$q''_x = -k \frac{dT}{dx} = -k C_1 = \frac{(T_{\infty,1} - T_{\infty,2})}{\left[\frac{1}{h_1} + \frac{1}{h_2} + \frac{L}{k} \right]}$$

2) Dik: Temperatur dan koefisien konveksi terkait dengan udara di dalam dan di luar permukaan dibelakang dinding

Dit: a) Temperatur di dalam dan di luar permukaan $T_{s,i}$ dan $T_{s,o}$

b) $T_{s,i}$ dan $T_{s,o}$ fungsi dari temperatur udara luar $T_{\infty,o}$ dan koefisien konveksi di luar.



Asumsi : 1) kondisi steady

2) konduksi satu dimensi

3) radiasi diabaikan

a) ~~hitung~~ baring konstant

$$q'' = \frac{T_{\infty,i} - T_{\infty,o}}{\frac{1}{h_o} + \frac{L}{k} + \frac{1}{h_i}} = \frac{25^{\circ}\text{C} - (-10^{\circ}\text{C})}{\frac{1}{10 \text{ W/m}^2 \cdot \text{K}} + \frac{0.004}{30 \text{ W/m}^2 \cdot \text{K}} + \frac{1}{30 \text{ W/m}^2 \cdot \text{K}}}$$

$$q'' = \frac{50^{\circ}\text{C}}{(0.154 + 0.0029 + 0.0333) \text{ m}^2 \cdot \text{K/W}} = 968 \text{ W/m}^2$$

$$T_{s,i} = T_{\infty,i} - \frac{q''}{h_i} = 25^{\circ}\text{C} - \frac{968 \text{ W/m}^2}{30 \text{ W/m}^2 \cdot \text{K}} = 7.7^{\circ}\text{C}$$

$$T_{s,o} = T_{\infty,o} + \frac{q''}{h_o} = -10^{\circ}\text{C} + \frac{968 \text{ W/m}^2}{10 \text{ W/m}^2 \cdot \text{K}} = 4.9^{\circ}\text{C}$$

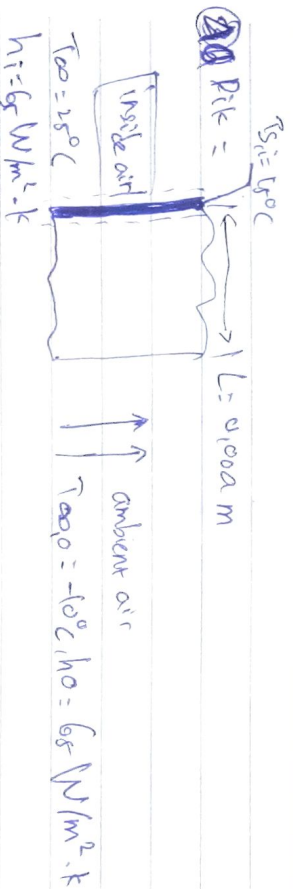


Table 3-4, Glass (300k) = $k = 1.4 \text{ W/m} \cdot \text{K}$

$$\frac{T_{\infty,i} - T_{s,i}}{1/h_i} + q''h = \frac{T_{s,i} - T_{\infty,o}}{L/k + 1/h_o}$$

$$q''h = \frac{T_{s,i} - T_{\infty,o}}{L/k + 1/h_o} - \frac{T_{\infty,i} - T_{s,i}}{1/h_i} = \frac{1^{\circ}\text{C} - (-10^{\circ}\text{C})}{\frac{0.004}{65 \text{ W/m}^2 \cdot \text{K}} + \frac{1}{10 \text{ W/m}^2 \cdot \text{K}}} - \frac{25^{\circ}\text{C} - 15^{\circ}\text{C}}{1}$$



$$q''h = (130 - 100) \text{ W/m}^2$$

$$= 1270 \text{ W/m}^2$$