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Ni/Al Layered Double Hydroxide Intercalated with Keggin Ion $[\alpha\text{-SiW}_{12}\text{O}_{40}]^{4-}$ for Iron(II) Removal in Aqueous SolutionAldes Lesbani^{2,3*}, Normah¹, Neza Rahayu Palapa³, Tarmizi Taher², Roy Andreas⁴, Risfidian Mohadi^{1,2}¹Department of Chemistry, Faculty of Mathematics and Natural Sciences, Universitas Sriwijaya, 30662, Indonesia²Research Center of Inorganic Materials and Coordination Complexes, Faculty of Mathematics and Natural Sciences, Universitas Sriwijaya, Palembang 30662, Indonesia³Graduate School of Mathematics and Natural Sciences, Faculty of Mathematics and Natural Sciences, Universitas Sriwijaya, Palembang 30662, Indonesia⁴Departement of Chemistry, Faculty of Mathematics and Natural Sciences, Universitas Jenderal Soedirman, Purwokerto 53123, Indonesia*Corresponding author email: aldeslesbani@pps.unsri.ac.id

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ABSTRACT. Layered double hydroxide (LDH) Ni/Al-NO₃ was synthesized using a coprecipitation method under base condition following with intercalation using Keggin ion $[\alpha\text{-SiW}_{12}\text{O}_{40}]^{4-}$ to form Ni/Al- $[\alpha\text{-SiW}_{12}\text{O}_{40}]$ LDH. The LDHs were characterized using XRD, FTIR, BET, and pH_{pzc} analyses. Furthermore, LDHs were applied as adsorbent of iron(II) from aqueous solution. The adsorption process was studied through the effect of adsorption time, the concentration of iron(II), and temperature adsorption. The results show the interlayer distance of LDHs was increased from 7.408 Å to 10.533 Å after intercalation process. The adsorption of iron(II) on LDHs showed that adsorption of iron(II) on both LDHs follows pseudo first-order kinetic model with R² value is close to one. The adsorption process was spontaneous, with adsorption capacity up to 36.496 mg g⁻¹.

Keywords: layered double hydroxide, Ni/Al, Keggin ion, adsorption, iron(II)**INTRODUCTION**

Water pollution from heavy metals has directly affected to ecological balance and also flora, fauna, and human health. The heavy metal wastewaters are produced from industrial applications such as electroplating process, smelting, metallurgical, and chemical processes. Therefore, the removal of heavy metal from wastewaters is crucial for environmental security and human health (Koju, Song, Wang, Hu, & Colombo, 2018). Various methods have been applied to remove heavy metal ions from a solution such as ion exchange, membrane filtration, coagulation, and adsorption (Taher, Mohadi, & Lesbani, 2018a). Among these methods, adsorption is an excellent method due to fast process, simple operation, low cost, and efficient removal (Imron, Said, & Lesbani, 2017). The efficiency process of adsorption depends on kinds of the adsorbent for the removal of heavy metals.

The wide range adsorbents have been used to remove heavy metal ions such as chitosan (Fan et al., 2018), cellulose (Fakhre & Ibrahim, 2018), zeolite (Qiu et al., 2018), bentonite, montmorillonite, and layered double hydroxide materials (Palapa, Mohadi,

& Lesbani, 2018). Layered double hydroxide (LDH) is inorganic layer materials consists of divalent M²⁺ and trivalent M³⁺ metal ions. There is a small anion between the layer depending on synthetic conditions such as sulfate, nitrate, carbonate, or chloride (Machado, Alves de Freitas, & Wypych, 2019). The general formula of LDH is $[\text{M}^{2+}_{1-x}\text{M}^{3+}_x(\text{OH})_2]^{x+}(\text{An}^-)_{x/n}n\text{H}_2\text{O}$ with M²⁺/M³⁺ is divalent and trivalent metal ions and An⁻ is interlayer anions with valence n. LDH has a positive charge net, and that charge is balanced with an anion, which is located on interlayer LDH (Carmelj, Ruengkajorn, Buffet, & O'hare, 2019). The unique properties anion on interlayer LDH can be exchanged with other anions to obtain specific properties of LDH using large anions such as complex compounds, heteropoly and isopolyoxometalate (Omwoma, Chen, Tsunashima, & Song, 2014).

The use of LDH as adsorbent of heavy metal ions has been tested by many researchers and have limitation such as low adsorbed capacity due to formation of aggregates which restrict its use widely. Thus, LDH should be improved to enhance the adsorption capacity. A new modified hydrotalcite-like

adsorbent FeMnMg-LDH has been applied as a potential material for the remediation of heavy metal contamination, such as Pb^{2+} . Mg-Fe LDH hollow nanosphere, which was prepared by one step thermal method, was used as adsorbent of heavy metal ions such as As^{5+} and Cr^{6+} with maximum adsorption capacity 176.6 mg g^{-1} for arsenic and 148.7 mg g^{-1} for chromium (Mubarak et al., 2018). Hierarchical porous Ni/Co LDH thermalization was applied an adsorbent of $Cr(VI)$ ion with adsorption capacity 99.9 mg g^{-1} at $30 \text{ }^\circ\text{C}$ (Hu et al., 2019). The complex compound of $Fe(CN)_6^{4-}$ was used as intercalant of Mg-Al LDH. These materials were applied as strip test detection of heavy metal ions (Wang, Sun, Fan, & Ai, 2016). Polyoxometalate $[PW_{10}Mo_2O_{40}]^{5-}$ was used as intercalant on Zn-Al LDH and this material was characterized using X-ray diffraction, infrared spectroscopy, and cyclic voltammetry (Bi, Xu, Xu, & Liu, 2011). On the other hand, Taher et al. (2019 a,b) was used Keggin type polyoxometalate $[\alpha-SiW_{12}O_{40}]^{4-}$ as intercalant of Ca/Al LDH. Intercalated Ca/Al- $[\alpha-SiW_{12}O_{40}]$ has the ability as adsorbent of cadmium(II) and iron(II) from aqueous solution. The advantages of polyoxometalates as intercalant of LDH are that cluster compounds have various oxidation states, structures and shapes, stable, enhancing adsorption capacity, increasing basal spacing, increase the surface area and also easy to synthesize (Lesbani & Mohadi, 2014). Thus, research intercalation of polyoxometalate onto LDH is intriguing material chemistry research until this decade.

In this research, polyoxometalate $[\alpha-SiW_{12}O_{40}]^{4-}$ was used as intercalant of Ni/Al- NO_3 LDH to form Ni/Al- $[\alpha-SiW_{12}O_{40}]$. Materials Ni/Al- NO_3 LDH and Ni/Al- $[\alpha-SiW_{12}O_{40}]$ were used as adsorbent of iron(II) from aqueous solution. Iron usually found in ground water and presents in iron(II) ion with high concentration (Zhang, Zhao, Jiang, Shan, & Lu, 2014). According Indonesian standard as drinking water (MCLs) for iron is 0.3 mg/L (Indonesian Minister of Health No.492/MENKES/PER/IV/2010). Therefore, it becomes necessary to remove iron(II) from wastewater by an appropriate methods before its releasing them into the environment. According to He, Qiu, , Hu, & Liu (2018) the modified LDH which containing polyoxometalate can be remove iron(II) from wastewater. The better adsorption efficiency should be obtained by adjusting ratio of metal ions in the laminates ranges $1 < n < 4$, the ratio of metal ions is large, resulting in a large aperture size. However, according to Han, Lu, Wei, Wang, & Duan, (2008), the interlayer anion of LDH can be enhancing ability for removal metal ion. Furthermore, the adsorption was studied through the investigation effect of adsorption time, the concentration of iron(II), and temperature adsorption. Then kinetic and thermodynamic parameters have been obtained to explain adsorption phenomena on LDH.

EXPERIMENTAL SECTION

Chemical and Instrumentations

Chemicals are supplied from Merck and Sigma Aldrich, such as nickel(II) nitrate, aluminum(III) nitrate, iron(II) chloride, sodium hydroxide, sodium carbonate, sodium tungstate, sodium metasilicate, and hydrochloric acid. Water was obtained from the water purification system containing Purite® ion exchange material. Characterization using X-ray powder analysis was conducted using XRD Rigaku Miniflex-600. The sample was scanned at 1 deg min^{-1} . Analysis using FTIR spectrophotometer was conducted using Shimadzu FTIR Prestige-21 using KBr Pellet and sample was recorded at wavenumber $400\text{-}4000 \text{ cm}^{-1}$. Determination of surface area analysis was conducted using adsorption-desorption Quantachrome apparatus at 77 K . Iron(II) was analyzed using UV-Vis spectrophotometer BioBase BK-UV 1800 PC spectrophotometer after complexation with 1,10-phenanthroline at wavelength 510 nm . Determination of pH pzc was conducted under acid-base condition using hydrochloric acid or sodium hydroxide in sodium chloride solution (Umh & Kim, 2014). Keggin ion of $K_4[\alpha-SiW_{12}O_{40}]$ was synthesized according to previously reported literature (Lesbani, Kawamoto, Uchida, & Mizuno, 2008).

Synthesis of Ni/Al- NO_3 LDH and Preparation of Ni/Al- $[\alpha-SiW_{12}O_{40}]$

Synthesis of Ni/Al- NO_3 LDH was conducted using the coprecipitation method at pH 10. Nickel(II) nitrate 0.3 M was mixed with aluminum(III) nitrate 0.1 M with an equal amount, and the mixture was constantly stirred. Sodium carbonate 0.3 M was added into the mix with the same amount of nickel-aluminum. The reaction was performed $80 \text{ }^\circ\text{C}$ for 17 hours under nitrogen flows. The pH was adjusted at pH 10 using the addition of sodium hydroxide 2 M . The solid green material was formed after 17 hours' reaction time. Green materials were washed several times with water and dried at $120 \text{ }^\circ\text{C}$ for 48 hours to form Ni/Al- NO_3 LDH (Li et al., 2010).

Preparation of Ni/Al- $[\alpha-SiW_{12}O_{40}]$ was conducted using an ion-exchange method. One-gram Ni/Al- NO_3 LDH in water was mixed with eight grams of $K_4[\alpha-SiW_{12}O_{40}]$. The reaction was performed under atmospheric nitrogen conditions for 24 hours. Material Ni/Al- $[\alpha-SiW_{12}O_{40}]$ was obtained and washed with water. Characterization of Ni/Al- NO_3 LDH and Ni/Al- $[\alpha-SiW_{12}O_{40}]$ was carried out using XRD, FTIR, BET, and pH pzc analyses.

Adsorption Studies

Adsorption was conducted using a small reactor batch system as similarly report by Taher, Rohendi, Mohadi, & Lesbani (2018b). The adsorption process was investigated by the effect of time, the effect of iron(II) concentration, and the effect of temperature. The influence of adsorption time was studied using

various time of adsorption at 10, 20, 30, 50, 70, 90, 110, 120, 150, and 180 minutes. The effect of iron(II) concentration was studied at 10, 15, 20, 25, and 30 mg L⁻¹. The effect of temperature adsorption was studied at 303, 313, 323, and 333 K. The final concentration of iron(II) was analyzed using UV-Vis spectrophotometer after complexation with 1,10-phenanthroline at 510 nm.

RESULTS AND DISCUSSION

Figure 1 shows XRD powder patterns of Ni/Al-NO₃ LDH (a) and Ni/Al-[α -SiW₁₂O₄₀] (b). Material Ni/Al-NO₃ LDH has unique diffraction at 11° (003), 24° (006), 35° (009), 40° (118), and 62° (110) as similarly report by JCPDS (No.15-0087). The well-ordered layer material of Ni/Al-NO₃ was identified at 11° (003), 24° (006), and 62° (110) (Zhang et al., 2019). Intercalation of Ni/Al-NO₃ LDH with K₄[α -SiW₁₂O₄₀] to form Ni/Al-[α -SiW₁₂O₄₀] resulting XRD as shown in **Figure 1b**. The main diffraction at (003) was shifted to a lower diffraction peak at 9° (003) due to the insertion of large anion onto interlayer distance. However, the reflection of (003) appeared in two diffractions at 9° and 11° denotes anion [α -SiW₁₂O₄₀]⁴⁻ might not be fully intercalated in interlayer, the impregnated has appeared. Similarly reported by Rives, Carriazo, and Cristina (2020) the macro-intercalant of LDH might not be successfully intercalated due to intercalation process which depends of LDH's matrix, pH and other treatments. Thao, Trung, & Van Long (2016) has been conducted Mg/Al LDH intercalated molybdate using starting treatments before intercalation process i.e., pre-swelling on solid LDHs and keep pH around 6.5. Other peaks were similar to Ni/Al-NO₃ LDH before intercalation. The interlayer distance at (003) before intercalation was 7.048 Å and after intercalation was

10.533 Å. Thus, intercalation of Keggin ion [α -SiW₁₂O₄₀]⁴⁻ onto interlayer distance of Ni/Al-NO₃ was successfully conducted. Kulandaivalu, Azman & Sulaiman (2020) was reported that the basal spacing of reflection (110) defines the unit cell which reflecting the distance between the two metal cations within the layers. The splitting peaks between (110) and (113) also defines the presents of anion in interlayer, usually this indicated the macro-anion (Han et al., 2008).

The FTIR spectra of Ni/Al-NO₃ and Ni/Al-[α -SiW₁₂O₄₀] LDHs were shown in **Figure 2**. The vibration of Ni/Al-NO₃ mainly contains three parts i.e., a vibration of nitrate (1600 cm⁻¹) and carbonate (1400 cm⁻¹) as ions on interlayer, a vibration of metal (670 cm⁻¹, 810 cm⁻¹), and vibration of water molecules (3400 cm⁻¹) (Gu, Huang, Wang, Yuan, and Ding, 2019). The intensity vibration of carbonate was very sharp before intercalation. The vibration of carbonate after intercalation was largely decreased due to the exchange ion process of carbonate to Keggin ion. The wavenumber at the range 900-1100 cm⁻¹ was also appeared due to the vibration of Keggin ion (vW=O, vW-O-W, vW-O-W, and vSi-O).

The nitrogen adsorption-desorption on Ni/Al-NO₃ and Ni/Al-[α -SiW₁₂O₄₀] LDHs is shown in **Figure 3**. There is an H3 hysteresis loop on Ni/Al-NO₃ and Ni/Al-[α -SiW₁₂O₄₀] LDHs with type IV isotherm curve. Materials were classifying as mesoporous materials (Kong & Adidharma, 2019). The BET analysis, as shown in **Table 1**, has largely increased of the surface area of Ni/Al-NO₃ to Ni/Al-[α -SiW₁₂O₄₀], indicating the opening of an interlayer distance of LDH. The pore volume and pore diameter of materials were also increased after the intercalation process.

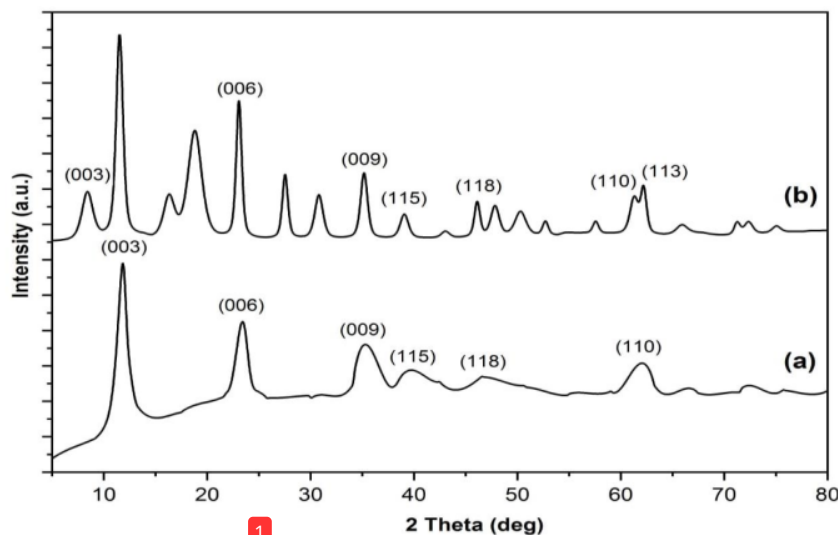


Figure 1. XRD powder patterns of Ni/Al-NO₃ (a) and Ni/Al-[α -SiW₁₂O₄₀] (b) LDHs

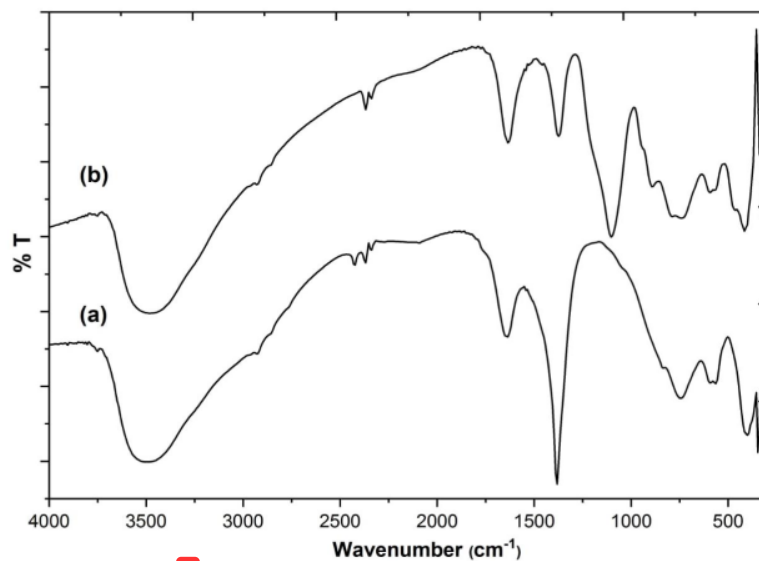


Figure 2. FTIR spectra of Ni/Al-NO₃ (a) and Ni/Al-[α -SiW₁₂O₄₀] (b) LDHs

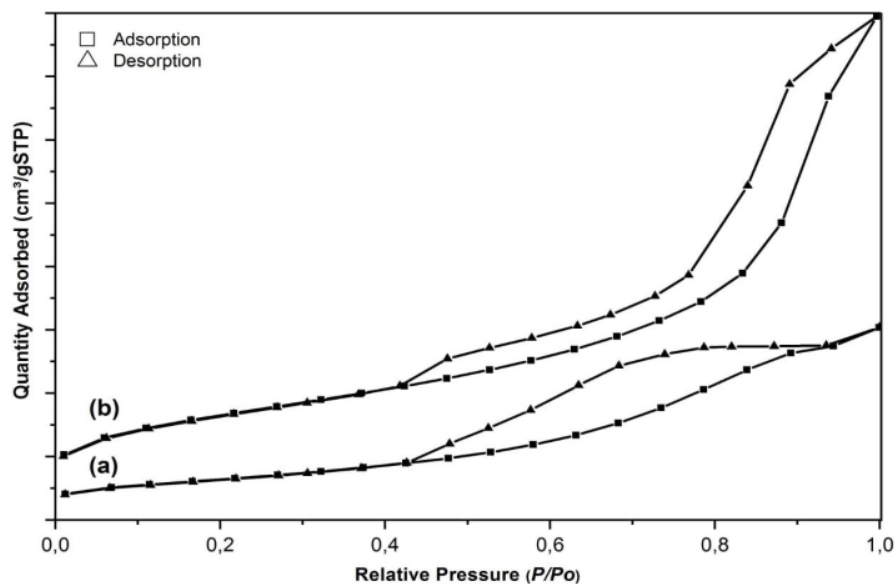


Figure 3. The BET isotherm profile of Ni/Al-NO₃ (a) and Ni/Al-[α -SiW₁₂O₄₀] (b) LDHs

Table 1. BET analysis of Ni/Al-NO₃ and Ni/Al-[α -SiW₁₂O₄₀] LDHs

Properties	LDHs	
	Ni/Al-NO ₃	Ni/Al-[α -SiW ₁₂ O ₄₀]
BET Surface Area (m ² g ⁻¹)	58.114	116.161
Pore volume (cm ³ g ⁻¹), BJH	0.118	0.237
Pore diameter (nm), BJH	7.405	9.629

The surface charges of Ni/Al-NO₃ and Ni/Al-[α-SiW₁₂O₄₀] LDHs were determined before materials used as adsorbent through the determination of p*H*_{pzc}. Both material Ni/Al-NO₃ and Ni/Al-[α-SiW₁₂O₄₀] have an intersection point at p*H* 8. The charges at that point are zero. The value below p*H*_{pzc} point has positive charges on the surface materials and vice versa. Thus adsorption of iron(II) on Ni/Al-NO₃ and Ni/Al-[α-SiW₁₂O₄₀] was conducted at p*H* 8.

The first process of adsorption was studied through the effect of adsorption time, as shown in Figure 5. The adsorption was gradually increased with increasing adsorption time and reach equilibrium at 120 minutes for both adsorbents. The kinetic pseudo first-order and pseudo second-order models were applied for data in Figure 1 (Oktriyanti Palapa, Mohadi, & Lesbani, 2019).

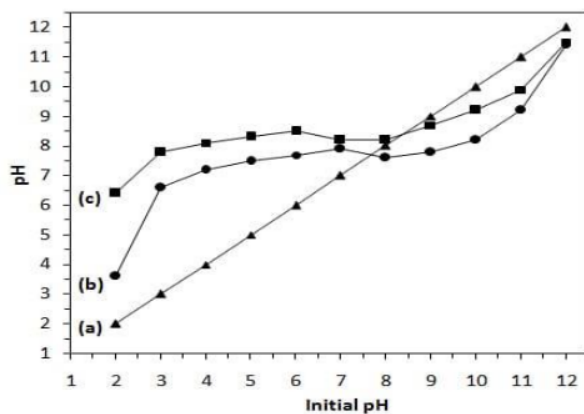


Figure 4. p*H*_{pzc} graph

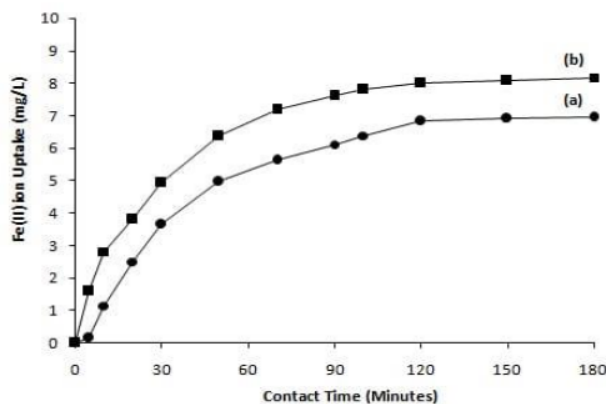


Figure 5. Effect of adsorption time of Ni/Al-NO₃ (a) and Ni/Al-[α-SiW₁₂O₄₀] (b) LDHs

Table 2. Kinetic Adsorption Model Ni/Al-NO₃ and Ni/Al-[α-SiW₁₂O₄₀]

Kinetic Adsorption Model	Kinetic Parameter	LDH	
		Ni/Al-[α-SiW ₁₂ O ₄₀]	Ni/Al-NO ₃
Pseudo First-Order	Q _e Exp (mg g ⁻¹)	8.178	6.947
	Q _e Calc (mg g ⁻¹)	14.385	7.881
	R ²	0.9055	0.9977
	k ₁ (min ⁻¹)	0.0447	0.0304
Pseudo Second-Order	Q _e Exp (mg g ⁻¹)	8.178	6.947
	Q _e Calc (mg g ⁻¹)	12.919	9.099
	R ²	0.305	0.987
	k ₂ (g mg min ⁻¹)	18.419	39.645

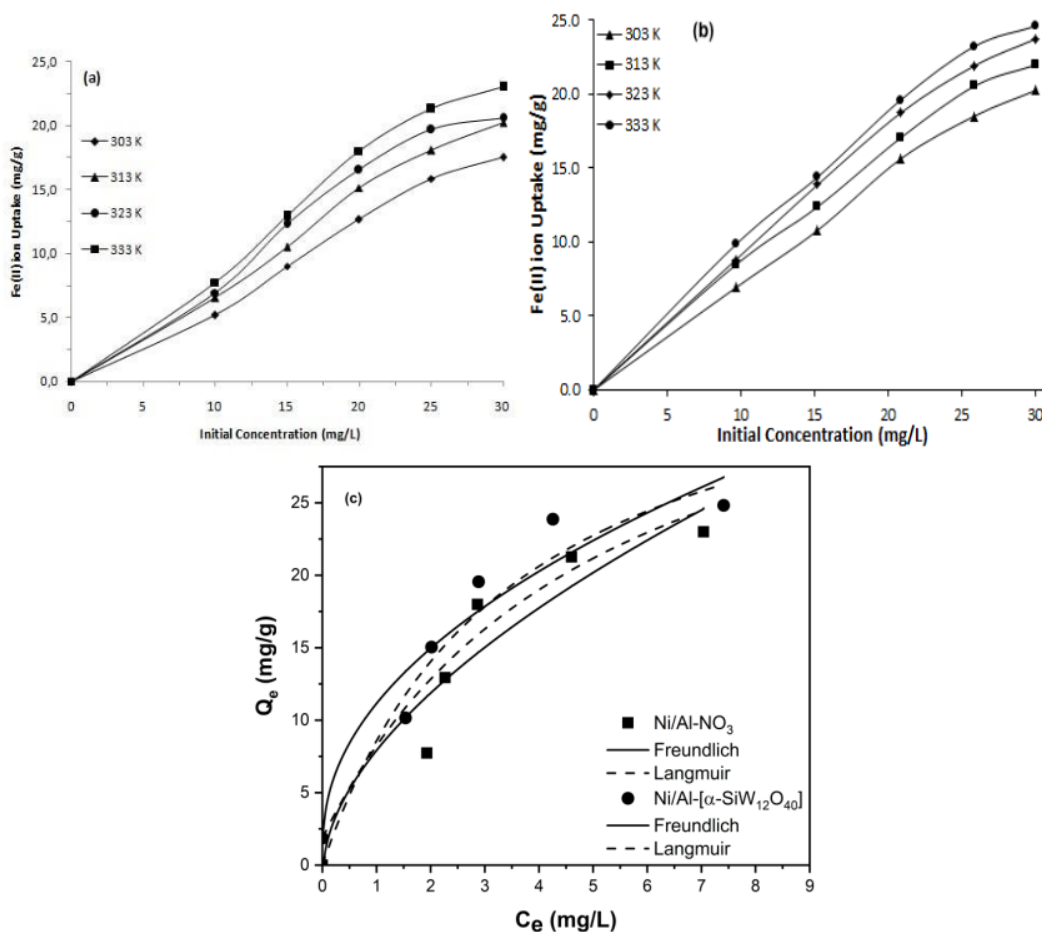


Figure 6. Effect of Concentration and temperature adsorption on Ni/Al-NO₃ (a), Ni/Al-[α-SiW₁₂O₄₀] (b) LDHs and isotherm adsorption (c)

Table 2 showed that the pseudo first-order kinetic model is appropriate for both adsorbents of Ni/Al-NO₃ and Ni/Al-[α-SiW₁₂O₄₀] LDHs and R² value is close to one. The k_1 value for Ni/Al-NO₃ and Ni/Al-[α-SiW₁₂O₄₀] LDHs are 0.0304 min⁻¹ and 0.0447 min⁻¹, respectively indicated material Ni/Al-[α-SiW₁₂O₄₀] LDH has higher reactivity to adsorb iron(II) from the aqueous solution than pristine material Ni/Al-NO₃ LDH.

The effect of concentration of iron(II) and the temperature of adsorption on Ni/Al-NO₃ and Ni/Al-[α-SiW₁₂O₄₀] is shown in Figure 6. The adsorption of iron(II) was increased by increasing concentration of iron(II) and by increasing temperature adsorption. Isotherm adsorption of iron(II) was calculated using Langmuir and Freundlich adsorption isotherm model as reported by Agarwal et al. (2016) was in Figure 6c and Table 3. The Freundlich isotherm fitted the experimental data better than Langmuir isotherm model, which indicated the adsorption was multilayer coverage as shown in Figure 6c. Table 3 showed that

the maximum adsorption capacity w_4 calculated by Langmuir equation obtained 60.241 mg/g for Ni/Al-NO₃ (303K) and 909.090 mg/g for Ni/Al-[α-SiW₁₂O₄₀] (303K). furthermore, the increasing temperature caused the adsorption capacity decreased. These findings indicated that LDH's interlayer is expanded and caused the iron molecule was difficult to adsorb. As similarly reported by Liao and Chen (2016) that the maximum adsorption capacity is favored in room temperature. Freundlich isotherm model for both LDHs is appropriate for adsorption of iron(II) on LDHs for all temperatures with R² value is close to one. Due to linearity R² of Langmuir isotherm model than adsorption capacity of iron(II) on LDHs is up to 36.496 mg g⁻¹ (R² = 0.834).

The effect of concentration and temperature adsorption in Figure 6 was also used to calculate the thermodynamic adsorption of iron(II) on Ni/Al-NO₃ and Ni/Al-[α-SiW₁₂O₄₀] LDHs. The thermodynamic data is presented in Table 4.

Table 3. Isotherm adsorption of iron(II) on LDH

	Isotherm	Isotherm Parameter	Temperature (K)			
			303	313	323	333
Ni/Al-NO ₃	Langmuir	q _{max} (mg g ⁻¹)	60.241	416.670	47.393	51.282
		k _{ML} (L mg ⁻¹)	0.020	0.006	0.094	0.131
		R ²	0.3032	0.0216	0.4075	0.4822
	Freundlich	k _F (mg g ⁻¹)(L mg) ^{1/n}	0.020	2.264	4.692	6.457
		n	0.829	0.998	1.378	1.376
		R ²	0.9626	0.9522	0.7247	0.7544
Ni/Al-[α-SiW ₁₂ O ₄₀]	Langmuir	q _{max} (mg g ⁻¹)	909.090	77.519	51.546	36.496
		K _{ML} (L mg ⁻¹)	0.002	0.044	0.103	0.258
		R ²	0.002	0.422	0.806	0.834
	Freundlich	k _F (mg g ⁻¹)(L mg) ^{1/n}	1.744	3.378	5.161	7.840
		n	0.947	1.149	1.324	1.630
		R ²	0.8912	0.9258	0.9441	0.8107

Table 4. Thermodynamic Parameter

	ΔG° (kJ mol ⁻¹)				ΔH° (kJ mol ⁻¹)	ΔS° (J mol ⁻¹ K ⁻¹)
	303 K	313 K	323 K	333 K		
Ni/Al-NO ₃	-0.885	-1.638	-2.391	-3.144	21.927	0.075
Ni/Al-[α-SiW ₁₂ O ₄₀]	-1.457	-2.028	-2.599	-3.170	15.839	0.057

The data in **Table 4** showed that adsorption of iron(II) on both Ni/Al-NO₃ and Ni/Al-[α-SiW₁₂O₄₀] LDHs was spontaneously processing with negative ΔG° value for all temperature conditions. The negative value of ΔS° shows to increase the randomness of the adsorption process between adsorbate iron(II) and adsorbent Ni/Al-NO₃ and Ni/Al-[α-SiW₁₂O₄₀] LDHs. The adsorption of iron(II) on both LDHs is categorized as physical adsorption with ΔH° value is less than 100 kJ mol⁻¹.

CONCLUSION

Material Ni/Al-NO₃ and Ni/Al-[α-SiW₁₂O₄₀] LDHs was successfully synthesized and used as adsorbent of iron(II) from aqueous solution. The adsorption of iron(II) on LDHs follows pseudo first-order kinetic model. The adsorption was categorized as physical adsorption with energy adsorption 15.893-21.927 kJ mol⁻¹, and adsorption capacity is up to 36.496 mg g⁻¹.

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